

# **GATE 2020**

## **Mechanical Engineering**

## **Forenoon Shift**

## Solution

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#### GENERAL APTITUDE

Ans. D
 Sol.
 Build : Building :: Grow : Growth
 Ans. D
 Sol.
 He is known for his unscrupulous ways. He always sheds crocodile tears to deceive people.
 Ans. B
 Sol.
 Ans. C
 Sol.
 Jofra Archer, the England fast bowler, is more fast than accurate.

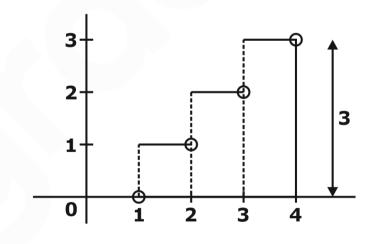
5.

Ans. D

Sol.

y = [x]

Area under the curve y = [x].



Area =  $1 \times 1 + 1 \times 2 + 1 \times 3$ 

= 1 + 2 + 3

= 6



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#### 6.

Ans. C

#### Sol.

Sucess Rate (P) =  $\frac{280}{500} \times 100 = 56\%$ Sucess Rate (Q) =  $\frac{330}{600} \times 100 = 55\%$ Sucess Rate (R) =  $\frac{455}{700} \times 100 = 65\%$ Sucess Rate (S) =  $\frac{240}{400} \times 100 = 60\%$ Average Success Rate =  $\frac{56 + 55 + 65 + 60}{4}$ = 59%

#### 7.

Ans. B

#### Sol.

Summery of the above paragraph

Funds raised through voluntary contributions on web-based platforms.

8.

Ans. C

Sol.

9.

Ans. C

Sol.

Sum of first n term is

= 8 + 88 + 888 + 8888 + .....

$$= 8[1 + 11 + 111 + 1111 + \dots]$$

$$=\frac{8}{9}[9+99+999+9999+....]$$







$$= \frac{8}{9} \Big[ (10-1) + (10^{2}-1) + (10^{3}-1) + (10^{4}-1) \Big]$$
  
$$= \frac{8}{9} \Big[ 10 + 10^{2} + 10^{3} + 10^{4} \dots n \Big]$$
  
$$= \frac{8}{9} \Big[ 10 + 10^{2} + 10^{3} + 10^{4} \dots n - (1+1\dots n) \Big]$$
  
$$\frac{8}{9} \Big[ 10 \cdot \frac{(10^{n}-1)}{10-1} - n \Big]$$
  
$$= \frac{80}{81} \Big( 10^{n} - 1 \Big) - \frac{8}{9} n$$

Ans. A

Sol. Put m = 2, so y = x<sup>2</sup> and y = 
$$x^{\frac{1}{2}}$$
  
And x= 0.5  
Y=x<sup>m</sup>= 0.5<sup>2</sup>= 0.25  
y=x<sup>1/m</sup> = 0.5<sup>0.5</sup>= 0.707  
so x<sup>1/m</sup> will be above than x<sup>m</sup>  
Satisfy option C.

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#### TECHNICAL

11.

Ans. C

Sol. Velocity for incompressible fluid flow,

$$\overrightarrow{V} = 2 \Big( x^2 - y^2 \Big) \hat{i} + V \hat{j} + 3k$$

From above velocity relation

$$u = 2(x^{2} - y^{2})$$
$$V = V$$
$$\omega = 3$$

If the flow is incompressible continuity equation has to be satisfied,

$$\frac{\partial u}{\partial x} + \frac{\partial V}{\partial y} + \frac{\partial \omega}{\partial z} = 0$$
$$\frac{\partial}{\partial x} \left( 2 \left( x^2 - y^2 \right) \right) + \frac{\partial V}{\partial y} + \frac{\partial}{\partial z} \left( 3 \right) = 0$$
$$\Rightarrow 4x + \frac{\partial V}{\partial y} + 0 = 0$$
$$\Rightarrow \frac{\partial V}{\partial y} = -4x$$
$$\Rightarrow \boxed{V = -4xy + C}$$

12.

Ans. (1.264)

Sol. Given

$C_1 = 1 mm$	$(HRC)_1 = 250$
C <sub>2</sub> = ?	$(HRC)_2 = 400$
$C=0.0032t\sqrt{\tau}$	
$C \propto \sqrt{C} \propto \sqrt{HRC}$	
$\frac{C_2}{C_1} = \sqrt{\frac{(HRC)_2}{(HRC)_1}}$	
$\Rightarrow \frac{C_2}{1} = \sqrt{\frac{400}{250}}$	
C <sub>2</sub> = 1.264mm	



Ans. A

Sol. Joule Thomson coefficient for real gas,

$$\mu = \left(\frac{\partial T}{\partial P}\right)_{h} = \frac{1}{C_{P}} \left[ T \left(\frac{\partial V}{\partial T}\right)_{P} - V \right] \dots (1)$$

For an ideal gas, PV = RT

$$T\left(\frac{\partial V}{\partial T}\right)_{P} - V$$
  
So,  $T\left(\frac{\partial V}{\partial T}\right)_{P} \times P = R$   
 $\left(\frac{\partial V}{\partial T}\right)_{P} = \frac{R}{P}$ .....(2)

Putting eqn (2) in eq (1)

$$\mu = \frac{1}{C_{P}} \left[ T \times \frac{R}{P} - V \right]$$

Now, since,  $\frac{12T}{P} = V$ 

$$\mu = \frac{1}{C_P} \Big[ V - V \Big] = 0$$

 $\mu = 0$  (for ideal gas)

14.

Ans. (244.94)

Sol. Pressure after  $1^{st}$  stage compression (P<sub>2</sub>) for perfect intercooling. Overall pressure ratio (r<sub>p</sub>) overall = 6

$$\left(r_{p}\right)_{overall} = \frac{P_{3}}{P_{1}}$$

For perfect intercooling, intermediate pressure (P<sub>2</sub>) =  $\sqrt{P_1P_3}$ 

 $P_1 = 100 \text{ kPa}$   $P_3 = 6P_1 = 600 \text{ kPa}$   $P_2 = \sqrt{100 \times 600}$  $= P_2 = 244.9 \text{ kPa}$ 

15.

Ans. (6)

Sol.  $\vec{A} = 2\hat{j} - 3\hat{k}$ ,  $\vec{B} = -2\hat{i} + \hat{k}$ 

 $\vec{C} = 3\hat{i} - \hat{j}$ 





$$\vec{A}(\vec{B} \times \vec{C}) = \begin{vmatrix} 0 & 2 & -3 \\ -2 & 0 & 1 \\ 3 & -1 & 0 \end{vmatrix}$$
$$= -2 (-3) - 3(2)$$
$$= 0$$
$$\therefore \vec{A}(\vec{B} \times \vec{C}) + 6 = 6$$

Ans. C

Sol.

Reynolds No.	Inertia force/Viscous force	
Grashoff	Buoyant/viscous	
Nusselt	Conv. H.T/cond. H.T.	
Prandtl No.	Momentum diffusivity /thermal diffusivity	

17.

Ans. A

Tds equation are

 $Tds = dU + pdv \rightarrow (1)$ 

 $\mathsf{Tds} = \mathsf{dU} + \mathsf{pdV} \not \rightarrow (2)$ 

From 1<sup>st</sup> Tds relation

Tds = dU + pdV

At constant volume, dV = 0

$$Tds = dU = CvdT$$

$$\frac{dT}{ds}\Big|_{V} = \frac{T}{C_{V}}$$
 at constant volume

So, at constant volume, slope of (T - S) is  $T/C_V$ From 2<sup>nd</sup> Tds relation, Tds = dH - vdP At constant pressure, dP = 0 Tds = dH = C<sub>p</sub>dT

$$\left(\frac{\partial T}{\partial S}\right)_{p=c} = \frac{T}{C_p}$$

So, ratio of slope of constant pressure & volume =  $\frac{T}{C_p} / \frac{T}{C_v} = \frac{C_v}{C_p}$ 

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Ans. C

Sol. The crystal of  $\boldsymbol{\gamma}$  iron (austenite phase) is FCC

19.

Ans. D

Sol. The normal force can be resolved into three components as shown in figure.

Due to  $f_a$  = axial force axial stress is Present in shaft

Due to  $f_T$  = thrust force torsion will be present in shaft.

Due to for bending stress.

But due to fu also bending will be there but in different plane to that due to hence bending stress in two planes.

20.

Ans. C

Sol.  $f(z) = \log z$ 

At z = 0

 $f(z) = \log z \Rightarrow$  not defined Hence out of all other functions logz is not analytic at z = 0.

21.

Ans. D

Sol. apply L hospital rule, you get answer as C/C+A.

It is direct formula of effectiveness in the case of counter flow heat exchanger when hate capacity ratio is 1

22.

Ans. C

Sol.  $\cos t \text{ time slope} = \frac{\operatorname{Crash} \operatorname{Cost} - \operatorname{Normal} \cos t}{\operatorname{Normal} \operatorname{time} - \operatorname{Crash} \operatorname{time}}$ 

23.

Ans. (49.33)

Sol. LMTD =  $\frac{\Delta T_1 - \Delta T_2}{\ell n \left(\frac{\Delta T_1}{\Delta T_2}\right)}$ 

```
\Delta T_1 = T_{hi} - T_{co} = 60^{\circ}
```

$$\Delta T_2 = T_{ho} - T_{ci} = 40^{\circ}$$

LMTD = 
$$\frac{60 - 40}{ln\left(\frac{60}{40}\right)} = 49.33$$
°C



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24. Ans. C

Sol. Froud Number is the ratio of inertia force/gravity force.

25.

Ans. B

Sol.

$$\begin{split} & \in = \frac{F_t}{F_0} \\ F_t = F_0 \Rightarrow \varepsilon = 1 \\ & \varepsilon = 1 \\ & \varepsilon = 1 \\ & \omega_n = 0 \Rightarrow \text{Not possible} \\ & \omega_n = \sqrt{2} \\ & \omega = \sqrt{2} \times \omega_n \\ & = \sqrt{2} \times \sqrt{\frac{k}{m}} \\ & \omega = \sqrt{\frac{2k}{m}} \end{split}$$

26.

Ans. D

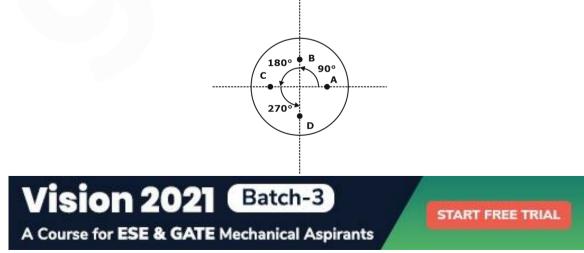
Sol.

Heat treatment process	Effect	
P: Tempering	B. Toughening	
Q: Quenching	C. Hardening	
R: Annealing	D. Softening	
S: Normalizing	A. Strengthening	

27.

Ans. (0.1)

Sol. If mass A is removed, then system becomes unbalanced.





F<sub>resultant</sub> = Net unbalanced force

$$= \sqrt{\left(\Sigma F_x\right)^2 + \left(\Sigma F_y\right)^2}$$
  

$$\Sigma F_x = mr\omega^2(\cos 90^\circ + \cos 180^\circ + \cos 270^\circ)$$
  

$$= mr\omega^2(0 - 1 + 0)$$
  

$$\Sigma f_x = -0.1$$
  
Similarly,  

$$\Sigma F_y = mr\omega^2(\sin 90^\circ + \sin 180^\circ + \sin 270^\circ)$$
  

$$\Sigma f_y = 0$$
  

$$F_r = \sqrt{\left(\Sigma F_x\right)^2 + \left(\Sigma F_y\right)^2}$$

 $F_r = 0.1N = Net unbalanced force.$ 

28.

Ans. D

Sol. 
$$Lf(t) = \frac{1}{S^2 + \omega^2}$$
  
 $L^{-1}\left(\frac{1}{S^2 + \omega^2}\right) = f(t)$ 

or

L sin at = 
$$\frac{a}{S^2 + a^2}$$
  
 $\therefore$  L sin  $\omega t = \frac{\omega}{S^2 + \omega^2}$   
 $\therefore$  L<sup>-1</sup> $\left(\frac{1}{S^2 + \omega^2}\right) = \frac{\sin \omega t}{\omega}$ 

29.

Ans. D

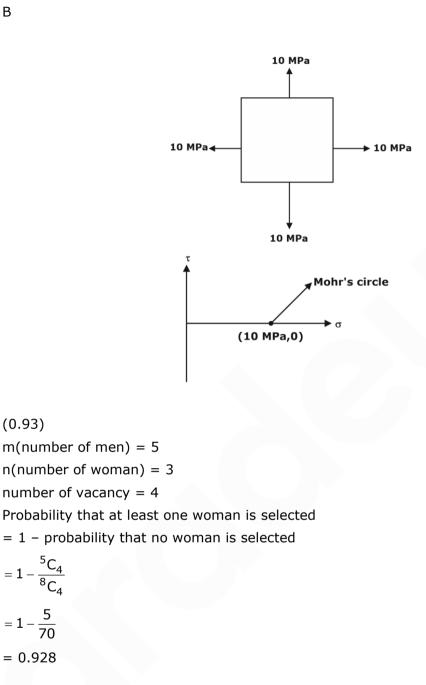
Sol. Matrix multiplication is Associative but not commutative.

eg. AB  $\neq$  BA But A (BC) = (AB) C  $\Rightarrow$  Associative



Ans. B

Sol.



32.

31.

Ans. (0.93)

 $=1-rac{{}^{5}C_{4}}{{}^{8}C_{4}}$ 

 $=1-\frac{5}{70}$ 

= 0.928

Ans. 1

```
\omega_{max} = 110 \text{ rad/s}
\omega_{min} = 100 \text{ rad/s}
\Delta E = A.05 \text{ kJ} = 1050 \text{ J}
I = ?
\Delta \mathsf{E} = \frac{1}{2} \mathrm{I}(\omega_{\max}^2 - \omega_{\min}^2)
```

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$$1050 = \frac{1}{2}I(110^2 - 100^2)$$
$$I = 1$$

Ans. D

For crank rocker, PQ should be shortest  $(s + I) \le P + Q$   $600 \text{ mm} \rightarrow \text{longest link}$  P = 300 mm, Q = 400 mm  $S + 600 \le (300 + 400)$  $S \le 100$ 

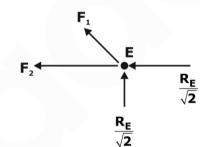
34.

Ans. C

Sol. Moment at A

$$(P \times 2\ell) = \frac{R_E}{\sqrt{2}} \times 4\ell$$
$$\Rightarrow R_E = \frac{P}{\sqrt{2}}$$

Pt. E



$$F_1 \sin 45^\circ + \frac{R_E}{\sqrt{2}} = 0$$
$$\frac{F_1}{\sqrt{2}} + \frac{R_E}{\sqrt{2}} = 0$$
$$F_1 = -R_E$$
$$F_1 = -\frac{P}{\sqrt{2}}$$

$$F_1 \cos 45 + F_2 + \frac{R_E}{\sqrt{2}} = 0$$

 $\frac{-P}{2}+F_2+\frac{P}{2}=0$ 



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 $F_2 = 0$ 

Correction option D

BF = 0

DH = 0

GC = 0

35.

Ans. D

Grinding  $\rightarrow$  for rough operations  $\rightarrow$  open structure wheels are preferred

0 to 16 so 12 will give more open

For rough operations brass tool with material is generally SiC

so C30Q12V will be the right choice

36.

Ans. B

Sol. r = 0.5 mm  $T_0 = 100^{\circ}\text{C}$   $T_{\infty} = 20^{\circ}\text{C}$   $T = 28^{\circ}\text{C}$  after t = 4.35 sec.  $\rho = 8500 \text{ kg/m}^3$   $C_P = 400 \text{ J/kgk}$  h = ?As it is lumped system

$$\frac{T - T_{\infty}}{T_0 - T_{\infty}} = e^{-\frac{hA}{\rho V C_p} \times t}$$

$$\frac{28-20}{100-20} = e^{-\left(\frac{h \times 4\pi r^2}{\rho \times \frac{4}{3}\pi r^3 \times C_p} \times t\right)}$$

$$\frac{8}{80} = e^{-\frac{h \times 4.35}{8500 \times \frac{0.5 \times 10^{-3}}{3} \times 400}}$$

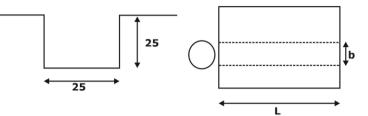
 $h = 299.95 \text{ w/m}^2 \text{k}$ 





Ans. (6.99)

Sol. Given



- D = 100 mm
- L = 300 mm
- b = 25 mm
- T = 20
- A (Approach) = 5 mm
- O (Overtravel) = 5 mm.
- d = 5 mm.

$$(f)_t = 0\% mm$$

Since d < slot dimension, the complete milling has to be done in 5 passes. Necessary approach = Necessary overtravel

$$= \frac{D}{2} - \sqrt{\left(\frac{D}{2}\right)^2 - \left(\frac{b}{2}\right)^2}$$

$$AN = \frac{100}{2} - \sqrt{\left(\frac{100}{2}\right)^2 - \left(\frac{25}{2}\right)^2}$$

$$AN = A.587 \text{ mm}$$
Time Per Cut
$$= \frac{L + AN + A + O}{f_T NT}$$

$$V = \pi D N$$

$$N = \frac{V}{\pi D} = \frac{35}{\pi \times 0.1}$$

$$N = 111.4 \text{ RPM}$$

$$(T)_{\text{per cut}} = \frac{300 + 1.587 + 5 + 5}{0.1 \times 111.4 \times 20}$$

$$(T)_{\text{per cut}} = 1.398 \text{ min.}$$
Total time = (T)\_{\text{per cut}} \times \text{ Number}
$$Total time = 1.398 \times 5$$

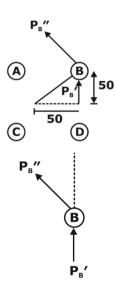
= 6.99 minutes



of cut



38. Ans. (16) Sol.

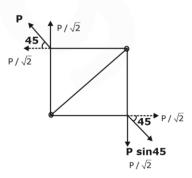


$$\begin{split} r_{B} &= \sqrt{50^{2} + 50^{2}} = 50\sqrt{2} \\ P_{B}^{'} &= \frac{P}{No. \text{ of bolt}} = \frac{10}{4} = 2.5 \text{ kN} \\ P_{B}^{''} &= \frac{P_{e}r_{B}}{\left(r_{a}^{2} + r_{b}^{2} + r_{c}^{2} + r_{d}^{2}\right)} \\ &= \frac{10 \times 10^{3} \times 0.4 \times \left(50\sqrt{2} \times 10^{-3}\right)}{4 \times \left(50\sqrt{2} \times 10^{-3}\right)^{2}} \\ &= 14.14 \text{ kN} \\ \text{Re sultant} = \sqrt{\left(P_{B}^{'}\right)^{2} + \left(P_{B}^{''}\right)^{2} + 2P_{B}^{''} \times P_{B}^{''} \cos 45^{\circ}} \\ &= 16 \text{ kN} \end{split}$$

39.

Ans. A

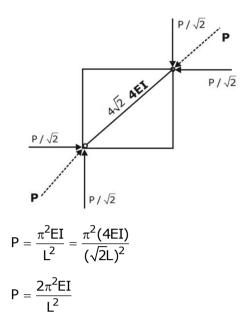
Sol.







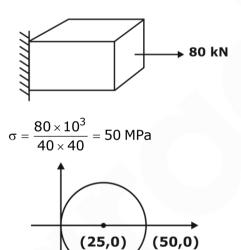
#### By shifting force

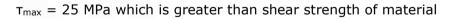


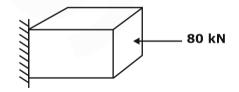


Ans. A

Sol.

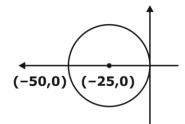




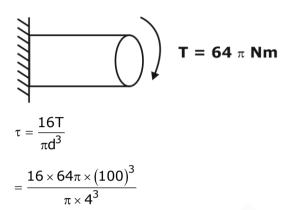


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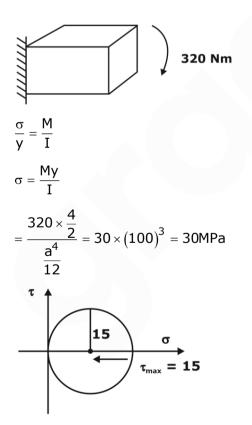




 $\tau_{max} = -25$  MPa which is greater than shear strength of material



 $\tau$  = 16 MPa which is less than shear strength of material



 $\tau$  = 15 MPa which is less than shear strength of material

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## 41. Ans. B Sol. $\Delta h = \mu^2 R$ $40 - 20 = \mu^2 \times 100$ $\mu^2 = \frac{20}{100} \approx 0.45$ $\mu = 0.45$ $1 - \frac{\Delta h}{D} = \cos \alpha \Rightarrow \cos \alpha = 1 - \frac{20}{200}$ a = 0.451Arc length = Ra = 100 × 0.451 Arc length 45.1 mm

42.

Ans. (2)

#### Sol.

$$\begin{split} f(z) &= (x^2 - y^2) + \xi (x, y) \\ Z &= 1 + i \\ x &= 1, y = 1 \\ \partial v &= \frac{\partial v}{\partial x} dx + \frac{\partial v}{\partial y} dy \end{split}$$

Those term of which not containing  $\boldsymbol{x}$  for analytic  $f^n$ 

$$\frac{\partial u}{\partial x} = \frac{\partial v}{\partial y}, \frac{\partial v}{\partial x} = -\frac{\partial u}{\partial y}$$

$$\Rightarrow u = x^{2} - y^{2}$$

$$2x = \frac{\partial v}{\partial y}, \frac{\partial v}{\partial x} = (-2y)$$

$$\frac{\partial v}{\partial y} = 2x, \frac{\partial v}{\partial x} = 2y$$

$$\frac{\partial v}{\partial y} = 2y, dx + 2x, dy$$

$$\begin{bmatrix} 0 \\ 0 \\ 0 \end{bmatrix}$$

$$\frac{\partial v}{\partial y} = 2y, dx$$

$$\frac{1}{0}$$

$$\frac{\partial v}{\partial y} = 2x, dy$$

$$\frac{1}{0}$$

$$\frac{\partial v}{\partial y} = 2x, dy$$

$$\frac{1}{0}$$

$$\frac{\partial v}{\partial y} = 2x, dy$$

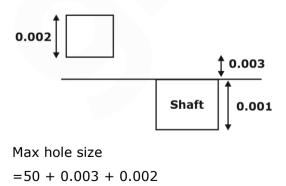
$$\frac{1}{0}$$





43. Ans. \* 44. Ans. (23.53)  $r = \frac{l_c}{l} = \frac{100}{250} = 0.4$ Shear angle,  $tan\phi = \frac{r\cos\alpha}{1 - r\sin\alpha}$  $=\frac{0.4\cos\bigl(20^\circ\bigr)}{1-0.4\sin\bigl(20^\circ\bigr)}$  $\phi = 23.53$ 45. Ans. (4) Sol. specific steam consumption (ssc) =  $\frac{3600}{W_{net}}$ Net work  $(W_{net})$  = Turbine work – Pump work = 903 - 3 = 900 KJ/Kg specific steam consumption =  $\frac{3600}{W_{net}}$ <u>= 360</u>0 900 = 4 Kg/Kwh 46. Sol.

Tolerance of hole = 0.002 mmTolerance of shaft = 0.001 mmallowance =  $0.003 \text{ mm} \Rightarrow \text{minimum}$ basic size = 50mm



= 50.005 mm





47. Ans. (-1) Sol.  $\mu(x) = \mu(y) = 0.5$  $\sigma^{2}(x) = \sigma^{2}(y) = 0.5 = 0.25$ Z = X + YVar(z) = var x + var y + 2 cov (x,y) $\therefore \operatorname{cov}(\mathbf{x}, \mathbf{y}) = \frac{-0.25 - 0.25}{2}$ = - 0.25  $\therefore r = \frac{cov(x,y)}{\sigma_x \sigma_y}$  $= \frac{-0.25}{\sqrt{0.25}\sqrt{0.25}}$ = - 1 48.

Ans. (B)

Sol.

div F = 
$$\frac{\left(x^{2} + y^{2} + z^{2}\right)^{\frac{1}{2}}}{\left(x^{2} + y^{2} + z^{2}\right)^{3}} \begin{bmatrix} -2x^{2} + y^{2} + z^{2} + x^{2} - 2y^{2} + z^{2} \\ +x^{2} + y^{2} - 2z^{2} \\ = 0 \end{bmatrix}$$
  
= 0  
$$\iint \vec{F} \cdot d\vec{s} = \iiint div F dv = 0$$

49.

Ans. (0.375)

Sol. Given

$$P_{1} = 0.36 \text{ KPa} \text{ (At Inlet)}$$

$$P_{2} = 0 \text{ (At outlet)}$$

$$A_{1} = 0.1 \text{ m2} \qquad \rho_{\text{air}} P_{0} = \frac{f_{x}}{A} = \rho v^{2} = A.2 \text{ kg/m}^{3}$$

$$A_{2} = 0.02 \text{ m2} \text{ [Constant]}$$

$$P_{0} = 2$$

Apply Bernoulli's equation at Inlet and outlet section.

$$\frac{P_1}{\rho_g} + \frac{V_1^2}{2_g} + Z_1 = \frac{P_2}{\rho_g} + \frac{V_2^2}{2_g} + Z_2$$
$$Z_1 + Z_2, \qquad P_2 = 0$$





$$\frac{P_1}{\rho_g} + \frac{V_1^2}{2_g} = \frac{V_2^2}{2_g} \quad \dots \dots \dots (1)$$

By Continuity equation.

$$\rho_{1} A_{1} V_{1} = \rho_{2} A_{2} V_{2}$$

$$\rho_{1} = \rho_{2}$$

$$V_{1} = \frac{A_{2}}{A_{1}} V_{2}$$

$$V_{1} = \frac{0.02}{0.1} V_{2}$$

$$V1 = 0.2 V_2$$

Putting in equation

$$\frac{360}{1.2} = \frac{V_2^2 - (0.2V_2)^2}{2}$$
$$300 = \frac{0.96V_22}{2}$$

$$V_2 = 25 \text{ m/s}$$

Apply Bernoulli's equation between 2 and 0.

$$\frac{P_2}{\rho g} + \frac{V_2^2}{2g} + Z_1 = \frac{P_0}{\rho g} + \frac{V_0^2}{2g} + \tau_0$$

$$Z_1 = z_0$$

$$P_2 = 0$$

$$V_0 = 0$$

$$\frac{V_2^2}{2g} = \frac{P_0}{\rho g}$$

$$P_0 = \frac{\rho V_2^2}{2}$$

$$P_0 = \frac{1.2 \times (25)^2}{2}$$

$$P_0 = 375 \text{ Pa}$$

$$P_0 = 0.375 \text{ KPa}$$
Sol. f(x) = x(x)  
a = -1  
b = 1.4

h = 0.6

50.

Sol.





number of Interval  $= \frac{b-a}{h} = \frac{1.4+1}{0.6}$ 

Уo	<b>y</b> 1	<b>y</b> 2	Уз	<b>y</b> n
-1	-0.16	0.04	0.64	A.96

By Simpson's 
$$\frac{1}{3}$$
rd Rule.  

$$\int_{-1}^{1.4} x |x| = \frac{h}{3} [y_0 + y_n + 2\{y_2\} + 4(y_1 + y_3)]$$

$$= \frac{0.6}{3} [-1 + 1.96 + 2(0.04) + 4(-0.16 + 0.64)]$$

$$= 0.592$$

#### 51.

Ans. (A)

Sol.

Production = 4 units  $2^{nd}$  case Production = 4 × 0.7 = 2.8 2.8 units % reduction =  $\left(\frac{4-2.8}{4}\right) \times 100$ = 0.3 × 100 = 30%

52.

Ans. (8)

Sol. Given

$$v = -c\left(r^{2} - \frac{D^{2}}{4}\right) = -c(r^{2} - R^{2})$$

$$v = c(R^{2} - r^{2})$$

$$d(KE) = \frac{1}{2}dm(v^{2}) = \frac{1}{2}v^{2}\rho dv = \frac{1}{2}\rho v^{2} \times v dA$$

$$d(KE) = \frac{1}{2}\rho v^{3} dA$$

$$KE\int d(KE) = \int \frac{1}{2}\rho c(R^{2} - r^{2})^{3} \times 2\pi r dr$$

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 $\begin{array}{l} \mathsf{KE} \propto \ \mathsf{R}^8 \\ \mathsf{KE} \propto \ \mathsf{D}^8 \end{array}$ 

53.

Sol.

Ans. (0.87)

U.PT

 $=\frac{1}{2}\rho c^{3}\int R^{6}+r^{6}-3R^{2}r^{2}-3R^{2}r^{2}(R^{2}-r^{2})2\pi rdr$ 

 $\frac{1}{2}^{2\pi\rho c^3}\int_{0}^{R}R^6r+r^7-3R^4r^3+3R^2r^5dr$ 

 $KE = npc^3 R^8 \times 0.625$  $KE = 0.625 \times npc^3 \times R^8$ 

 $KE \propto D^n \Rightarrow n = 8$ 

 $T_1 = \frac{\mu P}{3} \left( \frac{D^3 - d^3}{D^2 - d^2} \right)$ 

 $\mathsf{P}_1 = \frac{\mathsf{F}_1}{\frac{\pi}{4} \left(\mathsf{D}^2 - \mathsf{d}^2\right)}$ 

 $T_2 = \frac{\mu P}{4} (D + d)$ 

D = 250 mmd = 50 mm

 $\frac{P_1}{P_2} = 0.871$ 

54.

Sol.

Ans. (12.69)

 $\frac{T_{1}}{T_{2}} = \frac{\frac{\mu P_{1}}{3} \left( \frac{D^{3} - d^{3}}{D^{2} - d^{2}} \right)}{\frac{\mu P_{2}}{4} \left( D + d \right)}$ 



**C**<sub>r</sub> **C**<sub>r</sub> **C**<sub>b</sub>



 $\frac{P_1}{P_2} = \frac{\frac{(D+d)}{4}}{\frac{1}{3}\left(\frac{D^3-d^3}{D^2-d^2}\right)} = \frac{\frac{300}{4}}{\frac{1}{3}\left(\frac{250^3-50^3}{250^2-50^2}\right)} = \frac{75}{86.11} = 0.871$ 

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From, the above velocity diagram, Blade outlet angle ( $\beta$ ) can be found by,  $\tan \beta = \frac{C_f}{C_b}$  where,  $C_f$  is flow velocity  $C_b$  is blade velocity

Blade velocity (C<sub>b</sub>) = 
$$\frac{\pi D_{mean}N}{60}$$

$$=\frac{\pi\times 3\times 300}{60}$$

47.12 m/sec.

Flow velocity  $(C_f) = \frac{\text{volume flow rate}}{\text{net change in area}}$ 

Net change in area A.

$$= \frac{\pi}{4} \left( 4^2 - 2^2 \right)$$
$$= \frac{\pi}{4} \times \left( 16 - 4 \right)$$
$$= \frac{\pi}{4} \times 12 = 3\pi$$

Flow velocity (C<sub>f</sub>) =  $\frac{100}{3\pi}$  = 10.61m/sec So, blade outlet angle ( $\beta$ ),  $\tan \beta = \frac{C_f}{C_b} = \frac{10.61}{47.12} = 0.225$  $\beta = \tan^{-1}(0.225)$ 

$$\beta = 12.69^{\circ}$$

55.

Ans. (5.04)

```
Sol. Given
```

```
As = 125 cm2

As = 125 × 10<sup>2</sup> mm<sup>2</sup>

(\eta)<sub>cathode</sub> = 0.15

I = 12 + 0.2 t

t = 20 minutes.

C (Plating Constant) = B.5 × 10<sup>-2</sup> mm<sup>3</sup>/As

C = A.5 mm<sup>3</sup>/A min.

Since current is changing with time we have to Integrate

T \rightarrow thickness of coating
```

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$$\begin{aligned} \frac{dT}{dt} &= \frac{CI}{A_s} h_c \\ \frac{dT}{dt} &= \frac{(1.5)(12 + 0.2t)(0.15)}{125 \times 100} \\ dT &= \frac{(1.5)(12 + 0.2t)(0.15)dt}{125 \times 100} \\ T &= \int dT = \int_0^{20} \frac{(0.15)(1.5)(12 + 0.2t)dt}{125 \times 100} \\ T &= \frac{(1.5)(0.15)}{125 \times 100} \left[ 12t + \frac{0.2t^2}{2} \right]_0^{20} \\ T &= \frac{(1.5)(0.15)}{125 \times 100} [240 + 0.1 \times 400] \\ T &= 0.504 \times 10^{-2} \text{ mm} \\ T &= 5.04 \text{ }\mu\text{m} \end{aligned}$$

Ans. (48)

56.

Sol. Follower motion equation

$$y = 4(2\pi\theta - \theta^2)$$

Velocity,  $v = \frac{dy}{d\theta}$ = 8(n -  $\theta$ )

Acceleration,  $a = \frac{d^2y}{d\theta^2}$ 

= -8

For max. value of y,

 $\frac{dy}{d\theta} = 0$   $8(\pi - \theta) = 0$   $\theta = \pi$ for minimum value of y at  $\theta = 0, 2\pi$  $y = 0 = y_{min}$ 

 $R_{curvature} = R_{Base} + (y + a)_{min}$  $40 = R_{Base} + (0 - 8)$ 

 $R_{Base} = 48 \text{ mm}$ 



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57.

Ans. (4.51)

Sol. Thermal efficiency of Otto engine =  $1 - \frac{1}{(r)^{\gamma-1}}$ 

Where, r is compression ratio  $\eta = 1 - \frac{1}{(8)^{1.4-1}}$ 

= 0.5647 = 56.47 %

$$\eta = \frac{I.P}{Heat input}$$

Indicated Power (I.P) =  $\eta \times$  Heat input

=  $0.5647 \times 10 = 5.647$  kw

Mechanical efficiency  $(\eta_m) = \frac{\text{Brakepowe}(B.P.)}{\text{Indicatedpower}(I.P.)}$ 

$$0.8 = \frac{B.P.}{5.647}$$

B.P. = 4.51 kW

Brake power is 4.51 kW.

58.

- Ans. (A)
- Sol. m = 2 kg k = 5 N/m

By applying energy balance

$$\frac{1}{2}mv_{i}^{2} = \frac{1}{2}mv_{f}^{2} + \frac{1}{2}kx^{2}$$

$$= 2 \times (1.5)^{2} = 2 \times v_{f}^{2} + 5 \times (.4)^{2}$$

$$V_{b} = 1.360 \text{ m/s}$$

59. Ans. (10)

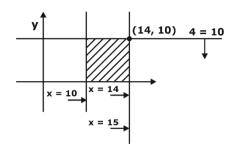
Sol. Let units of A = x





Let units of B = y

For Aakash.



X < 15

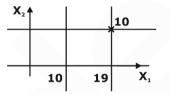
Given  $y \le 10$ 

But  $x \ge y$ 

 $10 \le x \le 15$ 

Given above the feasible regions max. revenue will happen at (15, 10)  $\therefore$  max revenue =  $14 \times 2000 + 10 \times 3000$  ......(i)

For Shweta



Let units of  $A = X_1$ 

Let units of  $B = Y_2$ 

Given  $X_2 \le 10 \ \& X_1 < 20 \ \& X_1 \ge X_2 \ge 10$ .

 $X_2 \le 10 \& 10 \le X_1 < 20.$ 

Maxima will occur at (19, 10).

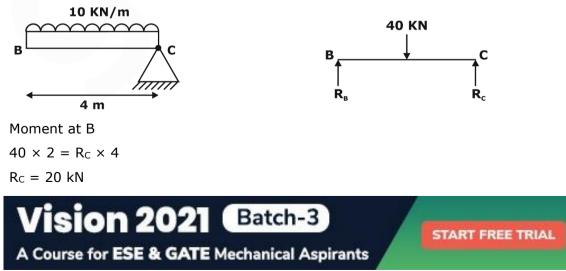
Max revenue =  $19 \times 2000 + 10 \times 3000$ ...... (ii)

Difference = (ii) - (i) =  $5 \times 2000 = 10000$  Rs. = 10 Thousands

60.

Ans. (20 kN)

Sol. Whenever we have internal hinge point, separate that portion





Sol. For a constant pressure process,

work done (W) =  $p(V_2 - V_1)$ 

\_

 $W = mR(T_2 - T_1)$ 

[from ideal gas, eqn. pV = mRT)

$$= mRT_1 \left[ \frac{T_2}{T_1} - 1 \right]$$
$$= 1 \times 0.287 \times 400 \left[ \frac{T_2}{T_1} - 1 \right] \dots (i)$$

Now, at constant pressure, Ideal gas eqn. becomes

$$\frac{\mathsf{V}_2}{\mathsf{V}_1} = \frac{\mathsf{T}_2}{\mathsf{T}_1}$$

Since,  $V_2 = 2V_1$ 

$$\frac{T_2}{T_1} = \frac{2V_1}{V_1}$$
$$\frac{T_2}{T_1} = 2$$

Putting eqn. (ii) in eqn. (i) we get .....

$$W = 1 \times 0.287 \times 400[2 - 1]$$

```
Ans. (1167.04 KN)
```

K = 210 MPa  
Hi = 20 mm  
H<sub>f</sub> = 15 mm  
R = 450 mm  
(V)<sub>R</sub> = 28 m/min  
B = 200 mm  
n = 0.25  
(
$$\sigma$$
)<sub>o</sub> =  $\frac{KE_T^n}{n+1}$ 

$$E_T = True Strain = In \frac{A_i}{A_f} = In \frac{I_f}{I_i}$$

 $A_i = B H_i$ 



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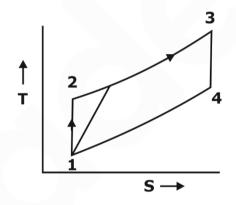
...(ii)



$$\begin{aligned} A_{f} &= B \ H_{f} \\ \epsilon_{T} &= ln \frac{H_{i}}{H_{f}} = ln \frac{20}{15} \\ \epsilon_{T} &= 0.2876 \\ \sigma_{o} &= Average \ flow \ stress = \frac{210.(0.2876)^{0.25}}{1.25} \\ \sigma_{o} &= 123.028 \ mPa \\ Rolling \ Force &= \sigma_{o}.I.B \\ l &= Contact \ length = \sqrt{R\Delta h} \\ l &= \sqrt{450 \times 5} \\ l &= 47.43 \ mm \\ f &= 123.028 \times 47.43 \times 200 \\ f &= 1167.04 \ KN \end{aligned}$$

```
Ans. (245 kJ/kg)
```

Sol. Temperature at inlet of compressor  $(T_1) = 310 \text{ k}$ 



For above (T-S) diagram of Brayton cycle,

 $Isentropic \; efficiency \; (\eta_{isen}) = \; 0.85 \; = \; \frac{Isentropic \; work}{Actual \; work}$ 

$$0.85 = \frac{h_2 - h_1}{h_2' - h_1}$$
$$h_2' - h_1 = \frac{h_2 - h_1}{h_2' - h_1} = \frac{C_p (T_2 - T_1)}{C_p (T_2 - T_1)}$$

$$n_1 = \frac{1}{0.85} = \frac{1}{0.85}$$

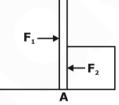
Now for (1 – 2) isentropic process =  $\frac{T_2}{T_1} = \left(\frac{P_2}{P_1}\right)^{\gamma-1/\gamma}$ 

 $\Rightarrow$  T<sub>2</sub> = 517.22k

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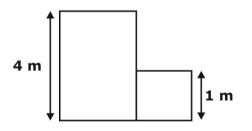
So actual difference in enthalpy  $(h'_2 - h_1) = \frac{C_p (T_2 - T_1)}{0.85}$   $= \frac{1.005(517.22 - 310)}{0.85}$  = 245 kJ/kg64. Ans. (105 KNm) Sol. Hydrostatic force in 1<sup>st</sup> & 2<sup>nd</sup> reservoir =  $\rho g A \overline{x}$   $A = h \times 1$  as width is unity A = h  $\overline{x} \rightarrow \text{centroid of centre of gravity}$   $= \frac{h}{2}$   $F_1 = F_2 = \rho g A \frac{h}{2} = \frac{\rho g h^2}{2}$   $F_1 = \frac{\rho g h_1^2}{2}$  $F_2 = \frac{\rho g h_2^2}{2}$ 



Moment around  $A = F_1 \times h^* - F_2 h^*$ 

Centre of pressure (h\*) =  $\frac{I_G}{A\overline{X}} + \overline{X}$ 

 $I_{G}=\frac{bh^{3}}{12}=\frac{h^{3}}{12}$ 



$$h^{*} = \frac{\frac{h^{3}}{12}}{h \times 1 \times \frac{h}{2}} + \frac{h}{2} = \frac{2h}{3}$$





Now this centre of pressure is from top from bottom distance of centre of pressure =  $\frac{h}{3}$ So, Net moment around A  $=\frac{1}{2}\rho gh_1^2 \times \frac{h_1}{3} - \frac{1}{2}\rho gh_2^2 \times \frac{h_2}{3}$  $=\frac{1}{2}\rho g \Bigg[\frac{h_1^3}{3}-\frac{h_2^3}{3}\Bigg]$  $=\frac{1000\times10}{2\times3}\Big[4^3-1^3\Big]$ = 105 KNm 65. Ans. (5.3%) Sol. Case 1 D = 1000 year T = 2 hrs. CP = Rs. 10 $Ch = \frac{10}{100} \times 10$ = Rs. 1  $T.C.1 = 10 \times 1000 + 480$  $= 10 \times 1000 + 400 + \frac{1000}{2} \times 1$ = 10000 + 400 + 500= 10900 Case II T = 6 minsCp = Rs. 5Ch = Rs. 5 $T.C.2 = 800 \times 10 + 2 \times 200 + \frac{800}{2} \times 1 + 200 \times 5 + \frac{6}{60} \times 200 + \frac{200}{2} \times 5$ = Rs. 10320 % reduction  $=1-rac{10320}{10900}$ = 0.053 = 5.3%



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